

**Prince of Songkla University**  
**Faculty of Engineering**

**Mid-Term Examination**

**20 December 2006**

**215-665 Energy from Biomass and Conversion**

**Semester 2/2549**

**Time 9:00-11:00**

**Room: A201**

**Directions**

- **This is close book examination.**
- **Dictionary is not permitted.**
- Calculator is permitted.
- Attempt all 5 questions.

**Juntakan Taweekun**  
**Instructor**

<b>Question</b>	<b>Marks</b>	
1	10	
2	10	
3	25	
4	10	
5	10	
Total	65	

Name \_\_\_\_\_

ID \_\_\_\_\_

Name \_\_\_\_\_ ID \_\_\_\_\_

**Question 1**

**1.1 Explain the meaning of the following items.**

- Biomass

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- Combustion

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- Stoichiometric Combustion

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- Higher Heating Value

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- Lower Heating Value

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Name \_\_\_\_\_ ID \_\_\_\_\_

**1.2 What are the advantages when using biomass residues as fuel instead of using fossil fuels? (No more than 7 answers)**

Name \_\_\_\_\_ ID \_\_\_\_\_

**Question 2**

There have several parts in biomass power plant. What are the main parts in the biomass power plant? Explain the working of each part and draw the connection of each part.

**Question 3**

In the palm oil mill, fiber is used as the fuel for boiler 40 Ton/hr. Use the following data for calculation of Questions 3.1 to 3.4.

<u>Fiber</u>		
- Total fiber from the process	11,500	kg/hr
- Excess fiber	3,246	kg/hr
- Low heating value	11,172.11	kJ/kg
<u>Boiler</u>		
- Operating pressure	21.5	bar (Saturated Steam)
- Temperature of raw water	29	°C
- Feed water to boiler	36	m <sup>3</sup> /hr
- Temperature of feed water	85	°C
<u>Ash</u>		
- Fly ash	350	kg/hr
- Bottom ash	82.15	kg/hr
<u>Blow Down</u>		
- Amount of blow down	7.08	m <sup>3</sup> /hr
- Temperature of blow down	98	°C
<u>Air</u>		
- Temperature of ambient air	26.6	°C
- Specific heat of ambient air	1.006	kJ/kg.°C
- Density of ambient air	1.178	kg/m <sup>3</sup>
- Air for combustion	33,814	m <sup>3</sup> /hr
<u>Flue Gas</u>		
- Temperature of flue gas	320.3	°C
- O <sub>2</sub> content from flue gas	11.4	%
<u>Radiation</u>		
- Coefficient of radiation (R)	1.1	
Reference air temperature	25	°C

**Find**

- 3.1 Calculate total energy input to boiler.
- 3.2 Calculate steam generation.
- 3.3 Calculate efficiency of boiler.
- 3.4 Draw Sankey Diagram and show the values for each energy loss in units of MJ/hr and Percent (%)

Name \_\_\_\_\_ ID \_\_\_\_\_

**Question 4**

Explain in details for the reducing formation of NO<sub>x</sub> by combustion measures.

Name \_\_\_\_\_ ID \_\_\_\_\_

**Question 5**

The following equation is “Dulong Formulation” for calculation of higher heating value ( $H_h$ ).

$$H_h = 8,080C + 34,200(H-O/8) + 2,500S$$

Derive the formulation by showing the obtained values of 8,080; 34,200; and 2,500.

TABLE A.1 Thermodynamic Properties of Steam

TABLE A.1.1 Saturated Steam: Temperature Table

Temp. Sat. °C	Press. Sat. kPa	Specific Volume <i>m</i> <sup>3</sup> / <i>kg</i>		Internal Energy <i>kJ/kg</i>			Enthalpy <i>kJ/kg</i>			Entropy <i>kJ/kg K</i>		
		Sat. Liquid <i>v<sub>f</sub></i>	Sat. Vapor <i>v<sub>g</sub></i>	Sat. Liquid <i>u<sub>f</sub></i>	Evap. <i>u<sub>fg</sub></i>	Sat. Vapor <i>u<sub>g</sub></i>	Sat. Liquid <i>h<sub>f</sub></i>	Evap. <i>h<sub>fg</sub></i>	Sat. Vapor <i>h<sub>g</sub></i>	Sat. Liquid <i>s<sub>f</sub></i>	Evap. <i>s<sub>fg</sub></i>	Sat. Vapor <i>s<sub>g</sub></i>
0.01	0.6113	0.001000	206.14	.00	2375.3	2375.3	.01	2501.3	2501.4	.0000	9.1562	9.1562
5	0.8721	0.001000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	.0761	8.9496	9.0257
10	1.2276	0.001000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	.1510	8.7498	8.9008
15	1.7051	0.001001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	.2245	8.5569	8.7814
20	2.339	0.001002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	.2966	8.3706	8.6672
25	3.169	0.001003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	.3674	8.1905	8.5580
30	4.246	0.001004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	.4369	8.0164	8.4533
35	5.628	0.001006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	.5053	7.8478	8.3531
40	7.384	0.001008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	.5725	7.6845	8.2570
45	9.593	0.001010	15.26	188.44	2248.4	2436.8	188.45	2394.8	2583.2	.6387	7.5261	8.1648
50	12.349	0.001012	12.03	209.32	2234.2	2443.5	209.33	2382.7	2592.1	.7038	7.3725	8.0763
55	15.758	0.001015	9.568	230.21	2219.9	2450.1	230.23	2370.7	2600.9	.7679	7.2234	7.9913
60	19.940	0.001017	7.671	251.11	2205.5	2456.6	251.13	2358.5	2609.6	.8312	7.0784	7.9096
65	25.03	0.001020	6.197	272.02	2191.1	2463.1	272.06	2346.2	2618.3	.8935	6.9375	7.8310
70	31.19	0.001023	5.042	292.95	2176.6	2469.6	292.98	2333.8	2626.8	.9549	6.8004	7.7553
75	38.58	0.001026	4.131	313.90	2162.0	2475.9	313.93	2321.4	2635.3	1.0155	6.6669	7.6824
80	47.39	0.001029	3.407	334.86	2147.4	2482.2	334.91	2308.8	2643.7	1.0753	6.5369	7.6122
85	57.83	0.001033	2.828	355.84	2132.6	2488.4	355.90	2296.0	2651.9	1.1343	6.4102	7.5445
90	70.14	0.001036	2.361	376.85	2117.7	2494.5	376.92	2283.2	2660.1	1.1925	6.2866	7.4791
95	84.55	0.001040	1.982	397.88	2102.7	2500.6	397.96	2270.2	2668.1	1.2500	6.1659	7.4159
100	101.35	0.001044	1.6729	418.94	2087.6	2506.5	419.04	2257.0	2676.1	1.3069	6.0480	7.3549
105	120.82	0.001048	1.4194	440.02	2072.3	2512.4	440.15	2243.7	2683.8	1.3630	5.9328	7.2958
110	143.27	0.001052	1.2102	461.14	2057.0	2518.1	461.30	2230.2	2691.5	1.4185	5.8202	7.2387
115	169.06	0.001056	1.0366	482.30	2041.4	2523.7	482.48	2216.5	2699.0	1.4734	5.7100	7.1833
120	198.53	0.001060	0.8919	503.50	2025.8	2529.3	503.71	2202.6	2706.3	1.5276	5.6020	7.1296
125	232.1	0.001065	0.7706	524.74	2009.9	2534.6	524.99	2188.5	2713.5	1.5813	5.4962	7.0775
130	270.1	0.001070	0.6685	546.02	1993.9	2539.9	546.31	2174.2	2720.5	1.6344	5.3925	7.0269
135	313.0	0.001075	0.5822	567.35	1977.7	2545.0	567.69	2159.6	2727.3	1.6870	5.2907	6.9777

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TABLE A.1.3 Superheated Vapor (Cont.)

<i>T</i>	<i>v</i>	<i>u</i>	<i>h</i>	<i>s</i>	<i>v</i>	<i>u</i>	<i>h</i>	<i>s</i>	<i>v</i>	<i>u</i>	<i>h</i>	<i>s</i>
	P = 1.60 MPa (201.41)				P = 1.80 MPa (207.15)				P = 2.00 MPa (212.42)			
Sat.	.12380	2596.0	2794.0	6.4218	.11042	2598.4	2797.1	6.3794	.09963	2600.3	2799.5	6.3409
225	.132 87	2644.7	2857.3	6.5518	.116 73	2636.6	2846.7	6.4808	.103 77	2628.3	2835.8	6.4147
250	.14184	2692.3	2919.2	6.6732	.12497	2686.0	2911.0	6.6066	.11144	2679.6	2902.5	6.5453
300	.158 62	2781.1	3034.8	6.8844	.140 21	2776.9	3029.2	6.8226	.125 47	2772.6	3023.5	6.7664
350	.174 56	2866.1	3145.4	7.0694	.154 57	2863.0	3141.2	7.0100	.138 57	2859.8	3137.0	6.9563
400	.19005	2950.1	3254.2	7.2374	.16847	2947.7	3250.9	7.1794	.15120	2945.2	3247.6	7.1271
500	.2203	3119.5	3472.0	7.5390	.19550	3117.9	3469.8	7.4825	.17568	3116.2	3467.6	7.4317
600	.2500	3293.3	3693.2	7.8080	.2220	3292.1	3691.7	7.7523	.199 60	3290.9	3690.1	7.7024
700	.2794	3472.7	3919.7	8.0535	.2482	3471.8	3918.5	7.9983	.2232	3470.9	3917.4	7.9487
800	.3086	3658.3	4152.1	8.2808	.2742	3657.6	4151.2	8.2258	.2467	3657.0	4150.3	8.1765
900	.3377	3850.5	4390.8	8.4935	.3001	3849.9	4390.1	8.4386	.2700	3849.3	4383.4	8.3895
1000	.3668	4049.0	4635.8	8.6938	.3260	4048.5	4635.2	8.6391	.2933	4048.0	4634.6	8.5901
1100	.3958	4253.7	4887.0	8.8837	.3518	4253.2	4886.4	8.8290	.3166	4252.7	4885.9	8.7800
1200	.4248	4464.2	5143.9	9.0643	.3776	4463.7	5143.4	9.0096	.3398	4463.3	5142.9	8.9607
1300	.4538	4679.9	5406.0	9.2364	.4034	4679.5	5405.6	9.1818	.3631	4679.0	5405.1	9.1329
	P = 2.50 MPa (223.99)				P = 3.00 MPa (233.90)				P = 3.50 MPa (242.60)			
Sat.	.07998	2603.1	2803.1	6.2575	.06668	2604.1	2804.2	6.1869	.05707	2603.7	2803.4	6.1253
225	.080 27	2605.6	2806.3	6.2639								
250	.087 00	2662.6	2880.1	6.4085	.070 58	2644.0	2855.8	6.2872	.058 72	2623.7	2829.2	6.1749
300	.09890	2761.6	3008.8	6.6438	.081 14	2750.1	2993.5	6.5390	.06842	2738.0	2977.5	6.4461
350	.109 76	2851.9	3126.3	6.8403	.090 53	2843.7	3115.3	6.7428	.076 78	2835.3	3104.0	6.6579
400	.120 10	2939.1	3239.3	7.0148	.099 36	2932.8	3230.9	6.9212	.084 53	2926.4	3222.3	6.8405
450	.130 14	3025.5	3350.8	7.1746	.107 87	3020.4	3344.0	7.0834	.09196	3015.3	3337.2	7.0052
500	.13998	3112.1	3462.1	7.3234	.116 19	3108.0	3456.5	7.2338	.099 18	3103.0	3450.9	7.1572
600	.15930	3288.0	3686.3	7.5960	.13243	3285.0	3682.3	7.5085	.11324	3282.1	3678.4	7.4339
700	.17832	3468.7	3914.5	7.8435	.14838	3466.5	3911.7	7.7571	.12699	3464.3	3908.8	7.6837
800	.197 16	3655.3	4148.2	8.0720	.164 14	3653.5	4145.9	7.9862	.140 56	3651.8	4143.7	7.9134
900	.215 90	3847.9	4387.6	8.2853	.179 80	3846.5	4385.9	8.1999	.154 02	3845.0	4384.1	8.1276
1000	.2346	4046.7	4633.1	8.4861	.19541	4045.4	4631.6	8.4009	.16743	4044.1	4630.1	8.3288
1100	.2532	4251.5	4884.6	8.6762	.21098	4250.3	4883.3	8.5912	.18080	4249.2	4881.9	8.5192
1200	.2718	4462.1	5141.7	8.8569	.226 52	4460.9	5140.5	8.7720	.194 15	4459.8	5139.3	8.7000
1300	.2905	4677.8	5404.0	9.0291	.242 06	4676.6	5402.8	8.9442	.207 49	4675.5	5401.7	8.8723