| Name   | Code |
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## PRINCE OF SONGKLA UNIVERSITY FACULTY OF ENGINEERING

Midterm Examination: Semester I

Academic year: 2007

Date: 5 August 2007

Time: 9.00-12.00

Subject: 230 – 425 Process Dynamics and Control

Room: R300

## ทุจริตในการสอบ โทษขั้นต่ำ คือ ปรับตกในรายวิชาที่ทุจริต และพักการเรียน 1 ภาคการศึกษา

• Only hand written note in a sheet of A4 and a dictionary are allowed.

• There are 9 pages of the exam.

• Write your name or your code on each page.

• If need to write the answers on the back of each page, please identify the problem number.

| Problem Number | Score |  |
|----------------|-------|--|
| 1              | 20    |  |
| 2              | 40    |  |
| 3              | 40    |  |
| 4              | 20    |  |
| 5              | 60    |  |
| Total          | 180   |  |

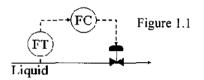
Dr. Kulchanat Prasertsit

Table 1 Laplace Transform

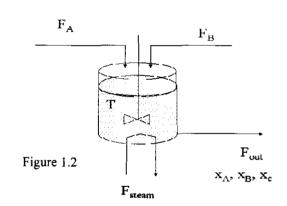
| F(s)   | f(t), t > 0  |
|--|--|
| $Y(s) = \int_0^\infty \exp(-st)y(t)dt$                         | f(t), t>0 $y(t)$   |
| Y(s)   | $y(t) = \frac{1}{j2\pi} \int_{c-j\infty}^{c+j\infty} \exp(st) Y(s) ds$ |
| $s^{n}Y(s) - s^{n-1}[y(0)]$                                    | nth derivative   |
| $-s^{n-2}[y'(0)] - \dots - s[y^{(n-2)}(0)]$ $-[y^{(n-1)}(0)]$  | y <sup>(n)</sup> (t)   |
| $\frac{1}{s}F(s)$  | $\int_0^t Y(\tau) d\tau$   |
| F(s)G(s)   | $\int_0^t f(t-\tau)g(\tau)d\tau$                                       |
| $\frac{1}{\alpha}F\left(\frac{s}{\alpha}\right)$ $F(s-\alpha)$ | f(at)  |
| F(s - α)   | $\exp(\alpha t) f(t)$  |
| $\frac{1}{s^2-\alpha^2}$                                       | $\frac{1}{\alpha}\sinh\left(\alpha t\right)$                           |
| $\frac{1}{s^2 - \alpha^2}$ $\frac{s}{s^2 - \alpha^2}$          | cosh(at)   |
| $\arctan\left(\frac{\alpha}{s}\right)$                         | $\frac{1}{t}\sin\left(\alpha t\right)$                                 |
| 1  | $\delta(t)$ , $\delta(t-\alpha)$                                       |
| exp (- αs), α 2 0  | $\delta(t-\alpha)$   |
| $\frac{1}{s}$  | u(t)   |
| $\frac{1}{s} \exp(-\alpha s)$                                  | u(t – α)   |
| $\frac{1}{s^n},  n = 1, 2, 3, \dots$                           | $\frac{t^{n-1}}{(n-1)!}$   |
| $\frac{1}{s+\alpha}$   | exp (- αt)   |
| $\frac{1}{(s+\alpha)^n}$ , n=1, 2, 3,                          | $\left[\frac{t^{n-1}}{(n-1)!}\right] \exp(-\alpha t)$                  |
| $\frac{\alpha}{s^2 + \alpha^2}$                                | sin (oxt)  |
| $\frac{s}{s^2 + \alpha^2}$                                     | cos(at)  |

| Name | Code |
|------|------|

- 1. (20 points)
  - 1.1 (10 points) Write "T" for correct statement and "F" for false statement (2 points for the correct answers and -1 point for incorrect answers)
  - a) \_\_\_\_Feed back control and feed forward control both require a measured variable.
  - b) The process variable to be controlled is measured in feedback control.
  - c) \_\_\_\_Feed forward control can provide perfect control: that is, the output can be kept at its setpoint even with an imperfect process model.
  - d) \_\_\_\_Feedback control will always take action regardless of the accuracy of any process model that was used to design it and the source of a disturbance.
  - e) Figure 1.1 is feed back control



1.2 (10 points) "Fresh feed A and fresh feed B are fed to CSTR with the flow rate of F<sub>A</sub> and F<sub>B</sub>, respectively. For safety reason, the level of the tank should not less

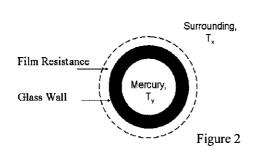


than 1/3 of the tank. And for economic reason, the concentration of  $x_C$  must be higher than 95%. At the moment the operator accidentally, opened valve for stream  $F_{Out}$  greater than its steady-state opening"

From the sentences classify all variables in the table below

| Controlled variables | Disturbance  | Manipulated variables |
|----------------------|--------------|-----------------------|
|                      |              |                       |
|                      | <del>-</del> |                       |
|                      |              |                       |
|                      |              |                       |

2. (40 points) The temperature of the mercury in mercury thermometer can be described in the following equation:



$$mC\frac{dT_{y}}{dt} = hA(T_{x} - T_{y})$$

m = mass of mercury in bulb

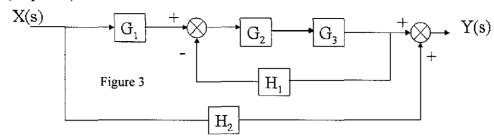
C = heat capacity of mercury

h = film coefficient of heat transfer

- 2.1 (10 points) Show how to get the equation and assumptions used for this problem.
- 2.2 (15 points) From the differential equation, use Laplace transform and deviation variable to find transfer function of  $T'_{y}(s) / T'_{x}(s)$ .
- 2.3 (15 points) If the changing in surrounding temperature is ramp function;

$$(T_x = T_x + b*t \colon t {\geq 0}$$
 ), find  $T'_y(t)$  and  $T'_y(\infty)$ 

3. (40 points)



- 3.1 (15 points) Find transfer function of Y(s)/X(s).
- 3.2 (10 points) Show characteristic equation of the process.
- 3.3 (15 points ) If  $G_1 = 1/(s+1)$ ,  $G_2 = (s+2)$ ,  $G_3 = 1/(3s+1)$ ,  $H_1 = 1$  and  $H_2 = 2$ , Find system order and find the steady-state value of Y(s) when x(t) = 5s(t)

- 4. (20 points) Process Response
  - 4.1 (10 points) The response of a liquid level in tank from a step change input is shown in the following figure. Answer the following question;

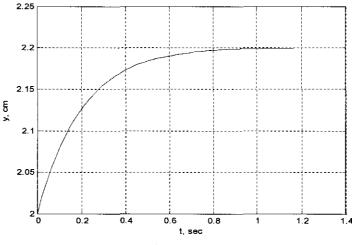
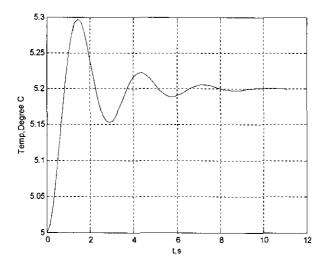


Figure 4.1

- a) What is the order of the system \_\_\_\_\_
- b) If the liquid input flow rate changes from 5 cm<sup>3</sup>/s to 7 cm<sup>3</sup>/s,

 $\tau_p = \underline{\hspace{1cm}}, K_p = \underline{\hspace{1cm}}$  Process Transfer function

4.2 (10 points) Figure 4.2 is the response of a tank temperature. The system is found as the 2<sup>nd</sup>-order. Answer the



following question

- a) Rise time =
- b) % Overshoot =\_\_\_\_
- c) Decay ratio = \_\_\_\_\_
- d) Settling time =\_\_\_\_
- e) Period =\_\_\_\_

5. (60 points) The process consists of 2-connecting tanks as shown in figure 5. Using deviation variables to

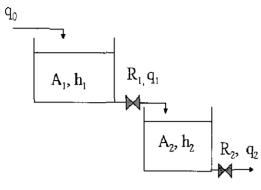


Figure 5

- 5.1 (30)Find transfer function;  $H_{2}^{'}(s)/Q_{o}^{'}(s)$
- 5.2 (20) Determine the process order, damping factor, process time constant and process gain.
- 5.3 (10) Does the process stable if the change in  $q_0$  is step function? Explain your answer.

(Let  $R_1 = h_1/q_1$ ,  $R_2 = h_2/\sqrt{q_2}$ ,  $q \equiv$  volumetric flow rate,  $A \equiv$  cross section area of each tank,  $h \equiv$  liquid level of each tank)